DESIGN AND IMPLEMENTATION OF A MEMS BASED SPIRAL CHANNEL DIELECTROPHORETIC SEPARATOR FOR CYTOMETRY APPLICATIONS

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ABSTRACT

DESIGN AND IMPLEMENTATION OF A MEMS BASED SPIRAL CHANNEL DIELECTROPHORETIC SEPARATOR FOR CYTOMETRY APPLICATIONS

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This thesis reports design and implementation of a MEMS based spiral channel dielectrophoretic separator for cytometry applications. Main objective of the thesis is to separate leukemia cells from healthy leukocytes with respect to the differences in their dielectric properties.

A novel MEMS based dielectrophoretic separator with spiral channels and concentric 3D electrodes has been proposed. The proposed geometry decreased the footprint, which reduces the device cost, without degrading the separation and quantization performances. Concentric electrode geometry enables continuous electric-field application with simple voltage supplies.

Theoretical explanation of the design has been presented and supported with finite element method simulations. Evolution of the design has been explained in conjunction with solutions to arising problems, chronologically. Comparisons of the proposed system with respect to the existing systems in the literature have been given.

The devices are fabricated using a 3-mask process utilizing suspended parylene channel process. The experiments are realized with 1 μ m and 10 μ m polystyrene beads. The results show that 1 μ m particles have an average speed of 4.57 μ m/s with 1.06 μ m/s standard deviation, and 10 μ m particles have an average speed of 544 μ m/s with 105 μ m/s standard deviation. The speed variation coefficient for 1 μ m and 10 μ m beads can be calculated as 23% and 19%, respectively. The size accuracy of the device is $\pm 10\%$, while the resolution is 20%, that is, particles with radii different from each other by 20% can be separated. It is worthy to note that the experimental results almost match the simulation results.

Keywords: Dielectrophoresis, separation, chromatography, cytometry, concentric electrodes, spiral channel, parylene, finite element method.

SİTOMETRİ UYGULAMALARI İÇİN MEMS TABANLI SPİRAL KANAL DİYELEKTROFORETİK AYRIŞTIRICI TASARIMI VE UYGULANMASI

Yılmaz, Gürkan Yüksek Lisans, Elektrik ve Elektronik Mühendisliği Bölümü Tez Yöneticisi: Doç. Dr. Haluk Külah

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Bu tez, sitometri uygulamaları için MEMS tabanlı bir spiral kanal diyelektroforetik ayrıştırıcının tasarımı ve uygulanmasını anlatmaktadır. Tezin temel amacı lösemi hücrelerini sağlıklı akyuvarlardan diyelektrik özelliklerindeki farklılıklara gore ayrıştırmaktır.

Spiral kanallara ve eşmerkezli üç boyutlu elektrotlara sahip MEMS tabanlı özgün bir diyelektroforetik ayrıştırıcı önerilmiştir. Önerilen geometri, ayrıştırma ve niceleme performansını kötüleştirmeden, aygıt fiyatını düşüren aygıt alanını küçültmüştür. Eşmerkezli elektrot geometrisi basit voltaj kaynakları ile sürekli elektrik alan uygulamasını mümkün kılmıştır.

Tasarımın kuramsal açıklaması sunulmuş ve sonlu eleman yöntemi ile desteklenmiştir. Tasarımın geçirdiği evrim, ortaya çıkan sorunlara getirilen

çözümlerle beraber kronolojik olarak açıklanmıştır. Önerilen sistemin literatürde varolan sistemlere gore karşılaştırılmasına yer verilmiştir.

Aygıtlar havada asılı parilen kanal sürecini kullanan 3-maskeli bir süreçte üretilmiştir. Deneyler 1 μ m ve 10 μ m polistiren boncuklarla gerçeklenmiştir. Deney sonuçları 1 μ m parçacıkların 4.57 μ m/s ortalama hız ve 1.06 μ m/s standard sapmaya, 10 μ m parçacıkların ise 544 μ m/s ortalama hız ve 105 μ m/s standard sapmaya sahip olduklarını göstermiştir. Sürat değişim katsayıları 1 μ m ve 10 μ m boncuklar için sırasıyla %23 ve %19 olarak hesaplanmıştır. Aygıtın boyut doğruluğu çözünürlük %20 iken ±%10'dur, yani yarıçapları birbirinden %20 farklı olan parçacıklar ayrıştırılabilir. Deneysel sonuçların benzetim sonuçlarıyla uyum sağlaması belirtmeye değer bulunmuştur.

Anahtar Kelimeler: Diyelektroforez, ayrıştırma, kromatografi, sitometri, eşmerkezli elektrotlar, spiral kanal, parilen, sonlu elemanlar metodu. To my family

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CHAPTER 1

INTRODUCTION

When integrated circuit (IC) production technology has been started to be applied to create electro-mechanical systems, Micro ElectroMechanical Systems (MEMS) research and application area has emerged. This research area exploits the microfabrication technologies developed for IC manufacturing and aims to create systems consisting of electrical and mechanical sub-systems. With this technology, macro level conventional applications such as accelerometers, gyroscopes, RF switches, bolometers, and pressure sensors are miniaturized at first for research purposes; however, nowadays most of them can be found in the customer electronics market. Besides, these micro sensors can be found in popular systems such as Apple iPhone and Nintendo Wii. This fast development line from research to end-product shows that MEMS technology will play an important role both in the cutting-edge technology development and in the customer electronics market in the very near future. This achievement can be explained by the following features which MEMS posssess:

- Small size (volume and mass)
- Low cost fabrication if mass production is available
- Low power consumption

In the last decades, MEMS technology found a new application area: Biomedical Micro ElectroMechanical Systems (BioMEMS). In this research and application area, basically, miniaturization of conventional biomedical systems and integration of these systems onto chips are studied. BioMEMS research can be analyzed in two classes: diagnostic and therapeutic [1]. Diagnostic systems cover analysis and

characterization of the biological samples, and therapeutic systems include flexible electrode arrays for stimulation and neural implants. This thesis concentrates on systems which can be utilized in diagnosis.

Ultimate goal in diagnostic BioMEMS is to design and implement systems which could perform the all the steps of a conventional clinical analysis on a single chip, so called Lab-On-a-Chip. As the name implies, BioMEMS offer chip-level biochemical laboratories, which are supposed to exhibit high performance at very low cost. In order to achieve this goal, first of all, the individual components have been studied, and now, integration of these components to perform an application is one of the main research topics in this area. These individual components refer to

- micro needles for injection and delivery purposes,
- various micro channel types for transportation and manipulation of fluids,
- micro valves, micro mixers, and micro pumps for microfluidic applications,
- micro grippers for handling a single cell
- gravimetric mass sensors for biological sample detection purposes,
- chemical and biochemical sensors for toxic agent detection, and
- electrical separators for separation and concentration purposes.

Currently, the researchers in BioMEMS area are looking for a way to combine the appropriate elements to design Lab-On-a-Chips performing a clinical analysis such as blood cell analysis, mutation detection, and cancer cell detection etc.

Another aspect of BioMEMS is to fulfill the necessity of micro level systems which possess dimensions comparable with the biological agents under consideration such as cell, bacteria, protein, and DNA. Note that micro systems allow realization of certain phenomena such as dielectrophoresis which is only applicable for particles in the range of 1 μ m - 1 mm and applications such as capillary electrophoresis which are not possible or feasible in macro level.

BioMEMS offer both massive and single particle analysis which is not common in conventional macro systems. Since cells or particles under concern in medicine and biology are in the order of micrometers, it is obvious that employing MEMS into biomedical systems is beneficial. A scaled diagram exhibiting common biological agents and their dimensions with respect to the dimensions employed in IC and MEMS fabrication technology is presented in Figure 1.1.

Other than these advantages, miniaturization of biomedical devices provides the below advantages additionally [2]:

- less sample and reagent consumption due to the analysis volume in the order of microliters,
- short analysis duration due to the shorter length of separation of concentration compared to conventional systems,
- safe experiments since chemical analytes which can cause hazardous reactions are used in very low volumes,
- enhanced heat transfer due to high surface area-to-volume ratio,
- in vivo usage since they are biocompatible and small enough to insert into the body,
- high sensitivity and resolution since the micro systems are comparable with the biological agents,
- laminar flow due to very low Reynolds number in the microchannels, and
- portability due to low weight and low power consumption.

Considering the mentioned advantages of BioMEMS over conventional biomedical systems, it is not surprising that biosensors have found applications in medicine, food safety, and homeland security.

As stated previously, devices performing separation of biological agents constitute one of the major research topics in the biomedical micro technologies. Separation of biological agents is generally the first step of many analyses. Note that the accuracy and the sensitivity of Lab-On-a-Chip systems can be improved by eliminating the unnecessary particles or concentrating the necessary particles at the very first separation step. Also, separation of biological agents is important for diagnosis in clinical medicine.



Figure 1.1: Scale comparison of biological agents vs. micro systems [3].

This thesis reports a dielectrophoretic particle and cell separator to differentiate different-size particles which possess the same electrical properties. Ultimate goal in this study is to enhance the performance of separation such that separation of subspecies of a cell line becomes possible due to their different sizes.

This chapter presents the literature survey related with separation methods and the background information on theoretical basis. Advantages and disadvantages of these methods have been compared for practical cases and the relevant discussions are presented.

Finally, the chapter is concluded with research objectives and motivations and organization of the thesis is given.

1.1 Particle Separation Methods and Theoretical Background

As explained previously, particle and cell separation methods constitute one of the most important research areas in BioMEMS. Therefore, various methods have been established through the years. Some of them are the imitations of the macro systems, and the rest is only possible for micro systems. General separation types employed in micro systems are based on acoustic, magnetic, mechanical, electrochemical, and electrical phenomena [4-5].

1.1.1 Acoustic Separation

Acoustic separation technique addresses the separation of particles by means of sound waves. Generation of standing waves via ultrasonic waves is the main method employed for acoustic separation which is also named as acoustophoresis. The main challenge in acoustic separation is to create and sustain the standing wave formation inside the channel which requires a challenging design phase and repeatable fabrication methods. Acoustic separation is performed via the trapping sites which correspond to the nodes and antinodes of the standing wave. The particles which are subjected to acoustic force move either towards the nodes or towards the antinodes depending on the particle properties. It has been reported that particles and cells which are under influence of acoustic forces are differentiated depending on their specific properties such as density or geometric properties such as size [6].

Since the positions and numbers of trapping sites are determined by the geometry of the separation chamber, the design phase is critical. Moreover, the deviations in the fabrication phase affect the device performance significantly. Note that separation efficiency degrades if the alignment of the trapping sites and separation zone is not perfectly done. An external resonator is required for generating a standing wave and integration of this external unit into the micro system is required. Therefore, to eliminate this requirement, acoustic separation is performed via surface acoustic waves which are generated on chip. Figure 1.2 presents the continuous particle

separation mechanism based on size difference using standing surface acoustic waves [7].



Figure 1.2: (a) Separation mechanism and repositioning of larger particles closer to the channel center and smaller particles farther from the center due to differing acoustic forces (b) Comparison of forces acting on particles at site 1 and site 2, respectively [7].

1.1.2 Magnetic Separation

Magnetic separation methods are mainly utilized for separation of ferromagnetic and non-magnetic particles. Note that using a magnet, ferromagnetic particles can be brought together, and therefore can be separated from non-magnetic particles. There are two methods employed to possess the magnetic property required for magnetic separation: either use the natural magnetic properties of the cell or attach a magnetic tag onto the cell [8]. The first one, usually, fails in the experimentation phase due to the weak magnetic properties of the living cells and non-magnetic polymeric beads. The latter one provides better separation performance; however, requires additional processing of the cell such as magnetic bead attachment protocols.

The most popular cell used in the literature is red blood cell due to its iron containing protein, Hemoglobin, content. Figure 1.3 shows the illustration of a red blood cell separator in continuous flow relying on magnetophoretic principles [9].



Figure 1.3: Schematic depiction of the micromagnetic separation device that contains a microfabricated layer of soft magnetic NiFe material adjacent to a microfluidic channel with two inlets and outlets [9].

1.1.3 Mechanical Separation

Differences in mechanical properties such as size, shape, and elasticity provide mechanical separation of particles. Common method is to create different size channels or different size obstacles to prevent the passage of bigger particles and allow the smaller ones [10]. Figure 1.4 presents an example of mechanical separation of particles depending on their size differences. Main challenge for this kind of design is the blockage of the gates due to piling bigger particles. Generally, turbulent flow regimes are created to prevent blockage; however, this solution increases the separation time and decreases the separation efficiency. Another way is to use the elasticity differences of the living cells. Common application is to differentiate red blood cells which exhibit a high elasticity from other blood cells.



Figure 1.4: Deep-field image of a filter array and access well. The 10 mm particles are arrested at the filter structures while 3 mm particles pass unaffected [10].

1.1.4 Electrochemical Separation

Miniaturization of the conventional macro systems such as voltammetry and amperometry defines the electrochemical separation methods. These systems detect the variations in the electrical signals due to the chemical reactions performed. Cell lysate impedance spectroscopy [11] is an example for electrochemical separation in which cell concentration is measured with respect to the variations in the lysing agent inside the solution. Figure 1.5 exhibits the experimental results of cell lysis by correlating the impedance variation with number of cells died. When the cells die, the content of the cytoplasm gets out and ion release from cell lysis causes impedance drop. As the cells die in this method, it is not suitable for systems which require further processing of the cells.



Figure 1.5: Impedance magnitude at 760 Hz during the process of cell capture and on-chip lysis. The impedance drop before and 10 min after injecting the lysing solution is associated with cell lysis and is used as a cell-numbers indicator [11].

1.1.5 Electrical Separation

Electrical separation methods rely on the differences in the dielectric properties of the particles and cells such as permittivity and conductivity. When permittivity and conductivity parameters are combined with the geometric information, capacitance and resistance values are found, respectively. Therefore, electrical modeling of the particles/cells and medium is performed with these parameters to understand the behavior. For instance, modeling of a living cell with its medium provides information about the reaction of the cell with respect to various concentration level of a certain ion to some extent.

Electrical separation is important since electrical properties of biological samples such as DNA and cells are specific to each type and these properties, generally, alter under unusual conditions. In the literature, there are mainly two electrical separation methods: electrophoresis and dielectrophoresis. All other methods in the literature can be deducted from these two methods. In fact, this classification depends on whether the particle has a net charge or not. Electrophoresis works on neutral particles. Electrophoresis, mainly, defines the movement of charged particles which are dispersed in a medium under a uniform electric field. Dielectrophoresis is defined as the movement of dielectric particles in the presence of a non-uniform electric field, when the particle and the surrounding medium have different dielectric constants and polarizabilities. Detailed information about electrical separation methods is supplied throughout the text. Figure 1.6 depicts a study on differentiation of white blood cells from yeast cells [12].



Figure 1.6: Separation of white blood cells and yeast cells using dielectrophoresis [12]. White blood cells are deflected to the angled micro channel due to the dielectrophoretic force generated at the tip of the triangular electrode whereas yeast cells continue to move in the mainstream.

Up to now, state-of-the-art separation methods in micro systems are explained briefly. In this study, electrical separation is preferred since it

- does not require labeling or magnetic tag attachment,
- is more reliable than acoustic separation thanks to its design and fabrication flexilibity,
- does not require electrochemical reactions to separate cells, and
- shows better performance than mechanical separation methods.

Next section describes the electrical separation methods reported in the literature and presents a comparison among them.

1.2 Electrical Separation Methods in the Literature

As indicated in previous section, electrical separation methods rely on the detection of the differences in the electrical properties of the particles and these techniques are mainly based on two electrical phenomena: electrophoresis and dielectrophoresis. Electrophoresis is the motion of charged particles, which are dispersed in a medium, under the influence of spatially uniform electric field. Dielectrophoresis is the motion of dielectric particles which have different polarizabilities from medium under spatially non-uniform electric field [13]. The main differences between electrophoresis and dielectrophoresis are observed in the definitions: Electrophoresis requires charged particles whereas dielectrophoresis can be performed on neutral particles since dielectrophoresis forms its own dipole from the polarizable particle. Moreover, uniform electric field is utilized in electrophoresis while non-uniform electric field is required in dielectrophoresis. This non-uniform electric field plays an important role in generating dipoles from neutral particles.

In order to separate particles using electrophoresis, particles should fit one of these options: either opposite charged particles or same charged particles which possess different amount of charge are required. Actually, the charge-to-mass ratio should be different to perform electrophoretic separation. Note that aggregation is inevitable when opposite charged particles are dispersed in a medium. Therefore, separation of opposite charged particles in the same medium is theoretically possible; however, practical problems are encountered during experimentation. On the other hand, separation of same charged particles which have different amount of charge is limited when resolution is considered. To increase resolution, separation length should be increased; however, it means higher voltage application to possess the same electric field magnitude, which is not practical. On top of that, it should be noted that most of the cells have a dynamic charge transfer with the ambient. Thus, relying on a constant net charge for separating cells is not reasonable. As a result, electrophoresis is not the best method for separation of particles. Nevertheless, power of electrophoresis in separation of charged particles such as DNA or proteins cannot be ignored [14]. When cells or polymeric particles are the main interest, dielectrophoresis steps up since it does not require a stable net charge distribution on the particle.

There are several types of dielectrophoresis reported in the literature: direct dielectrophoresis (DEP) [15-17], travelling wave dielectrophoresis (TWD) [18-19], electro-rotation (ROT) [20], isolating dielectrophoresis [21-22], image dielectrophoresis [23], and moving dielectrophoresis [24].

Direct dielectrophoresis has a number of advantages and differences with respect to the other types of dielectrophoresis. Firstly, travelling wave dielectrophoresis occurs where a travelling electric field exists. This existence can be provided by placing electrodes and applying phase-shifted signals to these electrodes. Therefore, controlled phase-shifted signal sources or phase shifter circuits are required to perform experiments. Secondly, electrorotation is an action induced by a dielectric dipole placed in a rotating electric field; therefore, it also requires phase shifted signals or high frequency switching on electrodes surrounding the region of interest. However, it should also be noted that electrorotation spectrum is very useful in determining dielectrophoretic spectra and extraction of DEP spectrum from ROT spectrum is very common in literature [25-26].

This extraction is necessary since directly measuring force exerted on cells is not possible, while extracting rotational speed of them using image processing tools is easy; however, this method still requires additional effort for image processing. Thirdly, isolating dielectrophoresis is an application of dielectrophoresis in which streaming and trapping regimes are employed. Dielectrophoretic streaming means the fluid flow through the arrays and trapping means the reversibly immobilization of particles on the insulating posts [21]. This method is similar to direct dielectrophoresis; however, immobilization process makes it a bit hard. Figure 1.7 shows fluorescence image of streaming dielectrophoresis of latex spheres in a microchip containing an array of diamond-shaped posts.



Figure 1.7: Fluorescence image of streaming dielectrophoresis of 200-nm fluorescent latex spheres (white) in a microchip containing an array of diamond-shaped posts (black) [21].

Fourthly, optical image-driven dielectrophoresis technique requires a photoconductive surface, on which electric fields can be patterned at high-resolution, for manipulation of particles [23]. Finally, moving dielectrophoresis utilizes moving electric field which is generated by sequentially energizing an array of electrodes to form an electric field that moves from one end to other as in the case of electrorotation [24].



Figure 1.8: Moving electric field is generated by sequentially energizing an array of electrodes to form an electric field that moves from one end to other. Note that there is no phase difference in the electric field, as in the traveling wave electric field [24].

From this point, direct dielectrophoresis will be named as dielectrophoresis since all the dielectrophoresis methods rely on almost the same theory. The only difference arises at real and imaginary parts of the Clausius-Mossotti factor which is a function of complex permittivities of the medium and the particle. Detailed analysis of Clausius-Mossotti factor is presented in Chapter 2.

1.3 Research Objectives and Thesis Organization

In this research, the following objectives are aimed:

- Design, simulation, and implementation of a dielectrophoretic cell separation system which does not require markers or labeling:
 - A design that satisfies the theoretical requirements of dielectrophoresis and could separate particles with respect to their size differences when the environmental conditions are properly adjusted.
 - A design that allows parallel processing, which means separation of various particles simultaneously.
 - Verification of the design with a simulation tool that utilizes finite element method. Comparison with rough hand calculations may be a good starting point to check the accuracy of the simulated model.
 - Fabrication flow development for the dielectrophoretic particle separator. The fabrication flow should be optimized at each step such that preceding and proceeding steps do not damage the current step.
 - Design of an experimental setup which aims to eliminate all the environmental effects that worsen the device performance and interfere with the device characterization.
 - Discussion of the experimental results in conjunction with the simulation results.

This thesis is organized as follows:

Chapter 2 introduces the theoretical background of dielectrophoresis with an emphasis on direct dielectrophoresis. Next, brief information about other types of dielectrophoresis, namely as travelling wave dielectrophoresis and electrorotation, is given. Then, strategies for application of dielectrophoresis are discussed by referencing the literature. Finally, techniques of dielectrophoresis are presented.

Chapter 3 gives the details of the design phase of the dielectrophoretic particle separator. First, the physical design of the separator is introduced with the discussion why this geometry is selected in comparison with other possibilities. Also, modifications on the design are presented by explaining the reasons. Next, theoretical explanation and validity of the final design is introduced with design parameters. Then, the trade-offs between the mentioned design parameters are investigated. After that, the advantages of this design are presented with practical reasons. Finally, simulations of the proposed structure are performed using finite element analysis tools to prove that the design is correct in terms of theoretical aspects such as electric field gradient and its distribution.

Chapter 4 spreads out the fabrication process of dielectrophoretic particle separator and experimentation. Fabrication flow is introduced in detail and solutions of the problems related with fabrication are explained. Fabricated devices, as well as the test setup, are presented. Next, the experimental method and the protocols for preparation of the samples are given. Finally, the test results are presented and discussions on the results in conjunction with simulation results are performed.

Finally, Chapter 5presents the conclusion of this work and states the possible future works related to this study. The final chapter explains the scientific value of this work and gives explicit examples for practical clinical applications. In the end, the methods that may enhance the separation performance are discussed.

CHAPTER 2

THEORY OF DIELECTROPHORESIS

Dielectrophoretic force is defined as the force exerted on an uncharged dielectric particle in the presence of a non-uniform electric field, when the particle and the surrounding medium have different dielectric constants and polarizabilities. Dielectrophoresis is the manipulation or the motion of particles which are exposed to the dielectrophoretic force.

Equation (2.1) represents the general formula governing the force (F) exerted on a dipole in an electric field (E), where (p) denotes the dipole moment of the particle and (∇) denotes the del operator in three dimensional Cartesian coordinate system [27].

$$\boldsymbol{F} = (\boldsymbol{p} \cdot \nabla)\boldsymbol{E} \tag{2.1}$$

The dipole moment of a homogenous solid spherical particle of radius R is defined in equation (2.2) [27]:

$$\boldsymbol{p} = 4\pi\varepsilon_m (\frac{\varepsilon_p^* - \varepsilon_m^*}{\varepsilon_p^* + 2\varepsilon_m^*}) \mathbf{R}^3 \boldsymbol{E}$$
(2.2)

where ε_m denotes the electrical permittivity of the medium, ε_p^* and ε_m^* are complex electrical permittivities of the particle and the medium, respectively.
2.1 Direct Dielectrophoresis (DEP)

Substituting equation (2.2) into equation (2.1) and assuming that applied electric field is formed via an AC source for the sake of generality, the time-averaged dielectrophoretic force exerted on a spherical particle is represented as [17]:

$$\langle F_{DEP} \rangle = 2\pi \varepsilon_m R^3 \operatorname{Re}(f_{CM}) \nabla |\mathbf{E}|^2$$
 (2.3)

where f_{CM} is the Clausius-Mossotti factor which indicates whether the medium or the particle is more polarizable as given in equation (2.4) [17].

$$f_{CM} = \frac{\varepsilon_p^* - \varepsilon_m^*}{\varepsilon_p^* + 2\varepsilon_m^*}$$
(2.4)

As stated previously, Clausius-Mossotti factor explains the dependence of the force on complex permittivities of the medium and the particle. Complex permittivity of the medium is defined as [17]:

$$\varepsilon^* = \varepsilon - j\frac{\sigma}{\omega} \tag{2.5}$$

where ω is the angular frequency of the applied electric field, and ε and σ denote the electrical permittivity and the electrical conductivity, respectively.

The definition in equation (2.5) holds for the particle; however, with a limitation. If the spherical particle is a homogenous rigid body, complex permittivity of the particle is defined as in equation (2.5). However, if the spherical particle is formed from a single shell covering a core, the particle complex permittivity, ε_p^* , equation becomes:

$$\varepsilon_{p}^{*} = \varepsilon_{s}^{*} \left[\frac{(\frac{R}{R-d})^{3} + 2(\frac{\varepsilon_{c}^{*} - \varepsilon_{s}^{*}}{\varepsilon_{c}^{*} + 2\varepsilon_{s}^{*}})}{(\frac{R}{R-d})^{3} - (\frac{\varepsilon_{c}^{*} - \varepsilon_{s}^{*}}{\varepsilon_{c}^{*} + 2\varepsilon_{s}^{*}})} \right]$$
(2.6)

where d is the thickness of the shell, R is the overall radius of the particle, and ε_c^* and ε_s^* denote the complex permittivities of the core and the shell, respectively. Figure 2.1 depicts a homogenous rigid spherical particle with radius R and a single shell spherical particle with overall radius R and shell thickness of d. More detailed modeling of alive cells is investigated in the literature [28].



Figure 2.1: (a) Homogenous rigid spherical particle with radius R and (b) single shell spherical particle with overall radius R and shell thickness of d.

Note that for multi-shell modeling purposes, complex permittivity definition gets more complicated; however, since most of the living cells can be modeled as a single shell and a single core, further calculation is not required at the moment. The hint for multi-shell modeling is to employ successive single shell operations from inner shell to the outmost shell.

The equations presented up to now gives the following outcomes:

- Under constant electric field, DEP force does not exist.
- Polarity of the applied potential is insignificant on the direction of the DEP force, therefore, direction of the DEP force can be either in the same direction with or in the opposite direction of electric field.

- Frequency of the applied potential plays an important role in the direction of the DEP force since the frequency is the only adjustable value in the complex permittivity equation. Note that complex permittivity defines the polarizability of the particle and the medium, and hence, the direction of the DEP force. If the particle and the medium have the same polarizabilities, force becomes zero.
- Force is directly dependent on the cube of the radius; however, it should be noted that dielectrophoresis is possible for particles having radii in the order of micrometers [17]. Thus, the application of the force is limited to micrometer scale particles.

Dielectrophoresis is classified as positive DEP or negative DEP depending on the sign of the f_{CM} which indicates the movement direction of the dielectric particle. If complex permittivity of the particle is larger than the medium, i.e. $\varepsilon_p^* > \varepsilon_m^*$, then the particle moves to the region where the electric field is more intense. Inversely, if complex permittivity of the particle is smaller than medium, i.e. $\varepsilon_p^* < \varepsilon_m^*$, then the particle moves to the region where electric field is less intense. These force direction dependent phenomena are called positive DEP (pDEP) and negative DEP (nDEP), respectively.

Limiting cases of the Clausius-Mossotti factor for frequency spectrum can be expressed as:

$$\lim_{\omega \to 0} \operatorname{Re}(f_{CM}) = \frac{\sigma_p - \sigma_m}{\sigma_p + 2\sigma_m}$$

$$\lim_{\omega \to \infty} \operatorname{Re}(f_{CM}) = \frac{\varepsilon_p - \varepsilon_m}{\varepsilon_p + 2\varepsilon_m}$$
(2.7)

The results show that the sign of the Clausius-Mossotti factor is determined by the electrical conductivities of the particle and the medium at low frequencies. However, it is determined by the permittivities at higher frequencies.

Figure 2.2 presents the variation of Clausius-Mossotti factor, and hence the dielectrophoretic force, with respect to the frequency of the applied electric field for different media conductivities.

Another point is that when frequency goes to zero (DC), if $\sigma_p \gg \sigma_m$, maximum value of the Clausius-Mossotti factor occurs and it is equal to 1. However, if $\sigma_m \gg \sigma_p$ occurs in the same case, then minimum value of the Clausius-Mossotti factor occurs and it is equal to -0.5. These outcomes can be extended for high frequency case when electrical permittivities are compared.

Careful analysis of the Clausius-Mossotti factor equation with complex permittivity definition shows that there exists a frequency such that the Clausius-Mossotti factor becomes zero, and therefore the DEP force. It is also evident that, at one side of this zero-force frequency the force is negative and at the other side, force is positive. This frequency is called *DEP crossover frequency*. The formal definition of DEP crossover frequency is that the point where the real part of Clausius-Mossotti factor, Re(f_{CM})becomes zero. The crossover frequency, f_{cross} , whose expression is given in equation (2.8) can easily be derived using above given formulas.

$$f_{cross} = \frac{1}{2\pi} \sqrt{\frac{(\sigma_m - \sigma_p)(\sigma_p + 2\sigma_m)}{(\varepsilon_p - \varepsilon_m)(\varepsilon_p + 2\varepsilon_m)}}$$
(2.8)

Analysis of Clausius-Mossotti factor indicates that separation of particles can be performed using the difference in their electrical properties. The distribution of crossover frequency for nine different types of tumor cells and normal peripheral blood mononucleocytes has been reported in the literature as depicted in Figure 2.3 [29]. For example, if 50 kHz signal is applied, monocytes will be affected by negative dielectrophoresis, whereas granulocytes will be affected by positive dielectrophoresis. The main challenge is, again, the resolution of crossover frequency.

Note that for particles or cells having crossover frequencies close to each other even if proper frequency is applied, dielectrophoretic forces may not be sufficient although they are in the opposite direction. Since the value of Clausius-Mossotti factor is close to zero near the crossover frequency, it will be wise to separate particles having sufficient difference in crossover frequency using this method. However, there is another way to separate particles possessing similar electrical properties: size based separation.



Figure 2.2: Variation of Clausius-Mossotti factor, and hence the dielectrophoretic force, with respect to the frequency of the applied electric field for three different media conductivities [12].

Considering that dielectrophoretic force is directly dependent on R^3 for a spherical particle, there exists a force difference for different size particles. At first, since mass is directly dependent on R^3 , it is not supposed to create any difference in acceleration terms.

However, it should be noted that when particle is exposed to dielectrophoretic force and starts to move, new forces arise and if all the forces acting on the particle are in balance, then no acceleration is observed, but this does not mean that there is no movement or the velocity is zero. Therefore, for zero acceleration case, a force balance equation can be designed by using the viscous drag force which is generated by the movement of the particle. Equation (2.9) denotes the viscous drag force [17].



Figure 2.3: Distribution of crossover frequency, a dielectrophoretic parameter, for 9 different types of tumor cells and normal peripheral blood mononucleocytes [29].

$$\overrightarrow{F_{drag}} = 6\pi\eta R\vartheta \tag{2.9}$$

where η denotes the viscosity of the medium and ϑ represents the velocity of the particle. Equating dielectrophoretic force and viscous drag force, force balance equation is obtained:

$$\overrightarrow{F_{DEP}} = \overrightarrow{F_{drag}}$$
(2.10)

Substituting the expressions of these two forces, the following equation is obtained:

$$2\pi\varepsilon_m R^3 \operatorname{Re}(f_{CM}) \nabla |\mathbf{E}|^2 = 6\pi\eta R\boldsymbol{\vartheta}$$
(2.11)

The velocity of the particle inside the microchannel can be derived from equation (2.11) by taking into account the effect of viscosity:

$$\langle \vartheta \rangle = \frac{\langle F_{DEP} \rangle}{6\pi R\eta}$$
 (2.12)

where $\langle \vartheta \rangle$ is the average velocity of the particles, R is the radius of the particle, and η is the viscosity of the medium.

According to equation (2.12), for two different particles having radii R_1 and R_2 and with Clausius-Mossotti factors $f_{CM,1}$ and $f_{CM,2}$, respectively, following relation between the average speeds $\langle \vartheta_1 \rangle$ and $\langle \vartheta_2 \rangle$ holds:

$$\frac{\langle \vartheta_1 \rangle}{\langle \vartheta_2 \rangle} = \frac{\frac{\langle F_{DEP,1} \rangle}{6\pi R_1 \eta}}{\frac{\langle F_{DEP,2} \rangle}{6\pi R_2 \eta}} = \frac{R_1^2 \operatorname{Re}(f_{CM,1})}{R_2^2 \operatorname{Re}(f_{CM,2})}$$
(2.13)

Therefore the average speed, or equivalently, the travelled distance in the microchannels for a predefined time period, can be used as the discrimination factor between different particles.

For the same type of particles having different sizes the expression becomes:

$$\frac{\langle \vartheta_1 \rangle}{\langle \vartheta_2 \rangle} = \frac{\frac{\langle F_{DEP,1} \rangle}{6\pi R_1 \eta}}{\frac{\langle F_{DEP,2} \rangle}{6\pi R_2 \eta}} = \frac{R_1^2}{R_2^2}$$
(2.14)

Since Clausius-Mossotti factors of the same type of particles will be the same, they will cancel each other.

As a result, for the particles having the same electrical properties, different size particles move at a velocity which is directly dependent of the square of their radii.

In this study, the main focus is on the separation of particles at different sizes, hence, derivations on the velocity vs. radius relationship has been derived from the alreadyestablished electrokinetic phenomena equations related with dielectrophoresis and viscous drag force.

2.2 Travelling Wave Dielectrophoresis (TWD)

Other component of the dielectrophoretic force causes the travelling wave dielectrophoresis. The difference between direct and travelling wave dielectrophoresis (TWD) is that direct dielectrophoresis requires magnitude gradient in the electric field, whereas TWD is observed under the presence of a phase

gradient. Since detailed background is presented in the direct dielectrophoresis section, this section will only introduce the differences. The common example is the one-dimensional travelling electric field (Figure 2.4) which is created by parallel microelectrodes. These electrodes are separated from each other such that there is a periodic distance, λ , between electrodes of the same phase. Therefore, the phase gradient is expressed as $2\pi/\lambda$ and induced force on the particle described in the previous sections is expressed as [13]:

$$\langle F_{TWD} \rangle = 2\pi \varepsilon_m R^3 Im(f_{CM}) E^2 \frac{2\pi}{\lambda}$$
 (2.15)

Note that imaginary of the Clausius-Mossotti factor is limited between -0.75 and 0.75 which exhibits a more balanced distribution when compared with the real part limitations. It is also obvious that all derivations related with speed are applicable to this case.



Figure 2.4: Illustration of one dimensional travelling electric field [17]. Since the signals on each electrode are shifted in time-domain, potential along the channel varies in space-domain at a certain instant. Therefore, the cell tracks the varying electric field.

2.3 Electrorotation

When a dielectric particle is subjected to an electric field, the particle gets polarized according to the orientation of the electric field. However, due to capacitive effects polarization of the particle requires a finite time. Consider a rotating electric field which is generated by means of utilizing a phase-varying non-uniform electric field. In this case, polarization orientation of the particle tries to follow the electric field orientation. Note that it lags the electric field with a certain time constant due to capacitive effects. If the electric field is adjusted to rotate fast enough, the polarized particle becomes misaligned with the electric field. The tendency of polarized particle to align itself with the electric field generates a net torque on particles. As a result, the dielectric particle starts rotating and will indefinitely rotate as long as the electric field rotates at a higher speed than particle polarization can achieve. This dielectrophoretic phenomenon is called electrorotation. As a result, electrorotation can be defined as the rotation of the polarized dielectric particle placed in a rotating electric field.

In contrast with electrophoresis, torque calculation is required for electrorotation instead of force calculation. Note that it is due to the rotational movement of the particles. The mathematical expression for the torque generated by electrorotation, given in equation (2.16), is directly dependent on the imaginary part of Clausius-Mossotti factor, $\text{Im}(f_{CM})$, in contrast with dielectrophoretic forces depending on real part, $\text{Re}(f_{CM})$.

$$<\Gamma_{ROT}>=-4\pi\varepsilon_m R^3 Im(f_{CM})|\mathbf{E}|^2$$
 (2.16)

It should be noted that there is also a crossover frequency where imaginary part of the Clausius-Mossotti factor becomes zero. This crossover frequency differentiates the rotation direction whereas the crossover frequency in real part case differentiates the movement direction. The rotation will be in the same sense with the rotating electric field when the actual frequency is below this crossover frequency; however, it turns opposite when the frequency exceeds this frequency. Considering the viscous drag forces associated with the particle an angular velocity for ROT can be defined as:

$$\Omega_{ROT}(w) = -\frac{\varepsilon_m \mathrm{Im}(f_{CM}) |\mathbf{E}|^2}{2\eta}$$
(2.17)

As stated previously, main application of electrorotation is to extract the dielectric parameters of the particles. Of course, there are also techniques aiming to use electrorotation directly to manipulate, examine, and differentiate cells [30-32].

2.4 Strategies for Applications of Dielectrophoresis

Since there exists many ways to create a non-uniform electric field to manipulate and separate particles, there are various strategies reported in the literature. This section presents the unique features of some popular strategies.

At first glance, it can be observed that creating different electrode configurations is the most common method to create a non-uniform electric field. Some of the electrode configurations can be listed as castellated electrodes [33], ratchet electrodes [34], concentric electrodes [35-37], and quadruple electrodes [38] for DEP; parallel and spiral electrodes [32] for TWD. These electrode configurations are investigated below.

2.4.1 Castellated Electrodes

This electrode configuration consists of electrodes which are patterned such that the distance between electrodes is periodically increasing and decreasing in a square wave formation. The electric field on the sharp edges of facing electrodes is intenser than the electric field formed in the inner regions of electrodes. Note that these electrodes can be placed with an off-set to manipulate the intense electric field regions. Figure 2.5 shows an example of castellated electrodes for dielectrophoretic force generation [33].



Figure 2.5: Castellated electrodes are utilized to create dielectrophoretic force. Separation of human metastatic breast cancer (larger cells) from dilute peripheral blood. (A) During initial collection. (B) During release. (C) Cancer cells remained on the electrode tips after blood cells had been swept downstream. (D) Close to the outlet only blood cells, in focused bands, are moving [33].

2.4.2 Ratchet Electrodes

This electrode configuration is patterned such that parallel electrodes are placed into the microchannel with a constant inclination angle with the wall of the microchannel. Since the electric field is stronger at the tips of the electrodes with respect to the regions near to the channel walls, positive DEP particles are confined into the middle of the channel and using a 3-way exit, these particles can be collected. Figure 2.6 illustrates the mentioned application [34].



Figure 2.6: An application of ratchet electrodes which separates cells using three-outlet system which differentiates focusing and deviating cells under electric field [34].

2.4.3 Concentric Electrodes

This electrode configuration provides a non-uniform electric field in the radial direction. Considering the electric field equation for coaxial lines, it is evident that strong electric field is generated around the inner electrode, whereas weak electric field is observed around outer electrode. This electrode configuration has an important aspect among the electrode configurations introduced in this section; there exists no fringe fields on the plane where electrodes are lying. This is due to the closed geometry of the structure. Unfortunately, this geometry makes the potential application to the inner electrode using co-planar metal routing very hard. However, this challenge is overcome by using a vertical wire along the normal line to the surface which does not cause disturbance in the field distribution in the region of interest.

Concentric electrode configuration is proposed in this thesis and relevant publications [35-37]. Figure 2.7 illustrates the concentric electrode configuration to create non uniform electric field in radial direction.



Figure 2.7: Concentric electrode configuration to create non uniform electric field in the radial direction [17].

2.4.4 Quadruple Electrodes

Quadruple electrode configuration consists of 4 electrodes facing a center point and each are offset by 90° with respect to each other. Electrodes are biased with sinusoidal voltages having a phase difference of 180° between the neighbour electrodes.

Therefore strong electric field is created along the gap between the electrodes and weak field is created at the center. Figure 2.8 shows an application of quadruple electrodes for manipulation and orientation of actin-myosin systems [38].



Figure 2.8: Quadruple electrodes are utilized to manipulate actin-myosin systems [38]. From left to right, no field application, distribution under electric field, and fluorescent imaging of actin-myosin systems are presented.

2.4.5 Parallel Electrodes

This electrode configuration consists of a series of parallel electrodes which are powered by signal having constant phase difference (Figure 2.9). Common method is to apply 0° , 90° , 180° , 270° , 0° , 90° ... cycle. This electrode configuration can be utilized for both direct dielectrophoresis and travelling wave dielectrophoresis by adjusting the phases of the applied signals.



Figure 2.9: An illustration presenting how direct and travelling wave dielectrophoresis can be applied using the same electrode configuration but changing the phases of the applied potential.

2.4.6 Spiral Electrodes

This electrode configuration can be utilized by either rectangular or spherical spiral electrodes. The structure is the wrapped version of very long parallel electrodes. Figure 2.10 exhibits a study where malaria infected erythrocytes are concentrated using 4 electrodes which are biased with 90° phase difference [32].



Figure 2.10: Collection of malaria infected erythrocytes by TWD. (A) Before application of a travelling electrical field, parasitised cells (arrows) were spread throughout the sample. (B) Application of four phase signals to the spiral electrode elements caused normal erythrocytes to be trapped at the electrode edges while parasitised cells were levitated and carried towards the centre of the spiral by the travelling field [32].

2.4.7 Insulating Obstacles and Deformations on the Channel

Up to now, methods of creating non-uniform electric field by electrode configuration is presented. Another way of forming a non-uniform electric field is to place insulating obstacles inside the channel which will disturb the field distribution. The insulating obstacle can be either inside the channel or at the channel wall. Figure 2.11 presents a study in which an insulating hurdle is constructed between the electrodes to create a non-uniform electric field to separate latex particles and yeast cells [12].



Figure 2.11: Utilization of an insulating hurdle to create non-uniformity in the electric field distribution [12].

Creating a non-uniform electric field is the first step to perform dielectrophoretic separation. However, correct solution and particle decision is another parameter that defines the separation performance. It should be remarked that it is required to use a solution which has a different polarizability from the particle at the separation frequency.

2.5 Techniques of Dielectrophoresis

Some applications of dielectrophoresis has become more popular than others and created a set of techniques such as field-flow fractionation and multiple frequency dielectrophoresis.

Field-flow fractionation is a time-domain separation technique that is reported a few decades ago. It states that application of a field causes separation due to the variation in the velocities of particles in different regions. Thus particles leave the microchannel at different speeds, and therefore at different types. For instance, when

particles are levitated with dielectrophoretic force, the particles at different heights will move along the channel at different velocities due to parabolic flow profile. Of course, channel length defines the separation resolution in this technique.

Multiple frequency dielectrophoresis is performed using electric fields at two or more frequencies [39]. Here, Clausius-Mossotti factor becomes dependent both the frequency and the location of the particle. Therefore, particles possessing similar Clausius-Mossotti factors can be separated by changing the effective f_{CM} . This technique can be utilized to cancel undesired dielectrophoretic traps and trap multiple groups of cells simultaneously.

CHAPTER 3

DESIGN OF THE DIELECTROPHORETIC PARTICLE SEPARATOR

This chapter focuses on the design of the dielectrophoretic particle separator. In the proceeding sections, firstly, physical structure of the device is presented. Next, theoretical explanation of the device is introduced by substituting the specific geometric formulations of the proposed structure into the governing equations of dielectrophoresis with emphasis on size based separation. After that, design parameters and trade-off between these parameters are explained. Finally, finite element method simulations are performed to validate and optimize the design.

3.1 Physical Structure of the Dielectrophoretic Particle Separator

The physical structure of a dielectrophoretic separator is based on two main components: the microchannel and the electrodes. Microchannels are utilized such that injected particles are confined in and separated throughout. Electrodes are the components which provide the required non-uniform electric field. As stated in Chapter 1, non-uniform electric field is required to create dielectrophoretic force. Common way of creating a non-uniform electric field is to adjust the electrode configuration. Basic method is to place parallel electrodes at different lengths. Thus, more intense electric field is created at the shorter electrode than the field intensity at the longer electrode as shown in Figure 3.1.



Figure 3.1: Parallel electrode configuration to create non-uniform electric field between electrodes.

In this study, non-uniform electric field in radial direction is created by means of concentric electrode configuration. Detailed explanation of the non-uniformity in the radial direction for this configuration is presented in section 2.3. This electrode configuration (Figure 3.2) is preferred due to several reasons: First of all, generated electric field is concentrated between the electrodes. Note that fringe fields are minimized in the co-planar surface with respect to parallel electrodes.



Figure 3.2: Concentric electrode configuration to form radially non-uniform electric field.

Secondly, continuous electric field exposure is possible if particles are placed between the concentric electrodes; actually, that is the case in this study.

The next step is to define the microchannels in which separation is performed. Instead of placing straight channels in the radial direction, spiral channel structure (Figure 3.3) is chosen due to several reasons: Firstly, layout area which will be used for microchannels is minimized by confining the spiral channels between the electrodes. On top of that, continuos exposure of electric field along the entire separation zone is achieved, as mentioned previously.



Figure 3.3: Red lines indicate the spiral channel walls and blue regions define the spiral channel area.

Final layout of the device is presented in Figure 3.11 in which spiral microchannels are confined between concentric electrodes. Note that Figure 3.11 just gives an idea about the top view of the device; however, there is the 3rd dimension which affects the performance of the device significantly. Therefore, modifications on 3D design

play an important role in the evolution of the dielectrophoretic separator. The next section introduces the modifications on the 3D design of the device.

3.2 Evolution of the 3D Device Design

Using the proposed layout, four different 3D level designs have been developed throughout the study. The modifications on the design are performed to

- solve the problems encountered in the fabrication,
- overcome the difficulties in the experimentation, and
- improve the performance of the separator.

Note that the design of the structures is initialized with layout drawing which is twodimensional design. In fact, the 3rd dimension evolves in the fabrication. Thus, all the modifications on the 3D design affect the fabrication significantly. Therefore, fabrication procedures of all four designs are explained in detail in Chapter 4 for the sake of completeness.

Evolution of the device is mainly based on the electrode placement in 3D since the major problem in concentric electrode configuration is to reach and bias the center electrode. First of all, cross junction electrode configuration is performed to bias the center electrode; next dome shaped center electrode configuration has been developed to solve the problems encountered in the first design. Thirdly, co-planar electrodes are proposed, and finally, the co-planar electrodes have evolved to 3D electrodes.

3.2.1 Design I: Cross Junction Center Electrode

Considering the layout of the device presented in Figure 3.11, a method to bias the center electrode has been proposed. This method involves a connection to the center electrode with electrodes having a "+" shape as indicated in Figure 3.4. Note that

biasing the outer concentric electrode is simpler since connection to that electrode does not intersect any other electrode.



Figure 3.4: Illustration of the cross-junction center electrode configuration: (a) top view and (b) side view.

In this electrode configuration, inner electrode and cross-junction connections are placed below the outer concentric electrode with an insulator in between them as depicted in Figure 3.4. Composition of the device is completed with the placement of the microchannel at the same level as the outer electrode. By keeping the insulator as thin as possible, amount of the electric field lines confined in the channel is supposed to be kept at maximum. However, this configuration has a significant problem that devastates the separation performance. The problem is based on an electrical phenomenon namely as dielectrophoretic trap. Dielectrophoretic trap occurs when the dielectric particle goes into a state where it cannot move any further. For instance, a negative DEP particle tends to move electric field minima. Therefore it moves from more intense electric field region to less intense electric field region. However, it cannot move any further if the path on the way is again a more intense electric field region. Note that particle tends to move to the less intense electric field region between these two more intense electric field regions independent of its movement direction. As depicted in Figure 3.5, the particle feels the strongest electric field at the inner and outer electrode junctions although that region is supposed to be the weakest electric field region according to the design. Moreover, the particle feels the weakest electric field in the center which is also the inverse of the proposed design. On top of that, the distribution of the electric field lines between concentric electrodes is disturbed and deviates a lot from what is supposed to be in this design. In order to solve the problem, cross junction connections have been removed and to bias the center electrode, dome shaped back side electrode configuration is proposed.



Figure 3.5: Weak and strong electric field regions in cross-junction center electrode configuration.

3.2.2 Design II: Dome Shaped Back Side Electrode

Instead of biasing the center electrode directly on the upper surface of the substrate, back side electrode formation is preferred in this modified design. Note that outer concentric electrodes are still placed on the upper surface of the substrate. Inner electrode is formed by shaping the substrate as a dome which reaches its peak at the center of the device where the center electrode is supposed to be placed. Figure 3.6 illustrates the inner and outer concentric electrodes from both top and bottom views. As Figure 3.6 presents, the outer electrode and inner electrode are placed on the front and the back sides of the substrate, respectively.



Figure 3.6: Illustration of the dome shaped back side electrode: (a) top view and (b) bottom view (c) side view.

In this design, placing an insulator between electrodes is not necessary in contrast with the first design. In fact, since the substrate material is chosen as glass for fabrication, it works as an insulator between two concentric electrodes to prevent short-circuit between electrodes. Figure 3.6 depicts the side view of the second design to provide a clear understanding of the structure.

This design solves the biasing problem for center electrode successfully. However, it is not the best solution since it has a repeatability problem in fabrication. On top of that, it has another crucial disadvantage: Electric field lines mainly confine into the glass layer between the concentric electrodes as illustrated in Figure 3.7, and hence, only fringe fields are confined into the channel and they are not sufficient to perform dielectrophoresis in this design.



Figure 3.7: Illustration of the electric field lines for design II. Electric field lines confine into the glass substrate instead of micro channels, therefore sufficient dielectrophoretic force cannot be generated inside the channels.

Since this design is performed to separate cells or particles in the order of several micrometers, the channel will be about 20 micrometers high. Therefore, fringe fields at a distance like this cannot create dielectrophoretic force which can overcome viscous drag force and move the particles. This problem is noticed during experimentation and at first fabrication method is tried to be optimized; however, it has been shown that, even if the thickness of the layer is minimized, device performance will not be sufficient by the finite element method simulations run

meanwhile. Therefore, this electrode configuration has to be replaced with a better one since experimentation of these devices yields no successful results. The next modification aims to confine the electric field lines into the channel as much as possible.

3.2.3 Design III: Co-planar Electrodes

From previous experience, it becomes evident that electrodes should be placed such that maximum number of electric field lines can confine into the separation zone, that is, into the spiral microchannels. The only way to provide this case is to place all the electrodes and the channel onto the same plane. This idea brings the third design which employs co-planar electrodes. In this design, inner and outer concentric electrodes are formed on the same plane and at the same height as a thin film. Then microchannels are confined between concentric electrodes. Figure 3.8 illustrates the top view and side view of the third design.



Figure 3.8: Illustration of the co-planar electrode configuration: (a) top view and (b) side view.

This design solves the electric field confinement problem, however, brings the contact problem to center electrode back. In this case, this contact problem is solved by taking an external help: probe tip. Using a "T" shaped probe tip connected to a micro manipulator, contact to the center electrode has been achieved. Figure 3.9 explains how the center electrode is biased using an illustration of the side view of the device. As shown in Figure 3.9, there is a height of "h" between the probe tip's side arm and the outer electrode. Since "h" is in the order of tens of millimeters and the distance between concentric electrodes is in the order of hundreds of micrometers, it can be ensured that the electric field lines confine into the microchannel at maximum.



Figure 3.9: Illustration of the method to bias the center electrode in co-planar electrode configuration.

This configuration solves all the previous problems; however, it has a minor disadvantage: since the electrodes are deposited as thin film metals, they are in the order of hundreds of nanometers. However, the channel height is in the order of 10-20 micrometers. Thus, upper portion of the channel contains fringe field lines and lower portion of the channel contains strong electric field lines. Therefore, another dielectrophoretic force in the z-axis is created. This force causes the particles to move either to the floor or ceiling of the channel depending on the dielectric parameters. Unfortunately, this effect is not desired and cannot be allowed in this design. The proposed dielectrophoretic separator is to be used in the separation of polymeric particles and living cells. However, the movement of the particles may be prevented since polymeric particles and alive cells have tendency to adhere another polymer which constructs the channel walls, parylene-C.

Therefore, the final modification takes place to remove the non-uniform electric field distribution in the z-axis throughout the microchannel.

3.2.4 Design IV: 3D Electrodes

Final design involves 3D electrodes which are placed in the same plane with the microchannels. The top view of this design is exactly the same as the third design, and there is just a slight difference between the side view of the final and the third design. Again, the contact to the center electrode is provided via external probe tip usage. As explained in the third design, the height of the electrodes is not comparable with the height of the microchannel. Thus, in the final design, the heights of the electrodes and the microchannel have been equalized to get better performance from the separator. Figure 3.10 introduces the side view of the final design.



Figure 3.10: Illustration of the side view of the 3D electrodes design.

Up to now, conceptual design of the dielectrophoretic separator is presented. In the next sections, theoretical explanation of the device will be presented with design parameters.

3.3 Theoretical Explanation of the Device

Conceptual design of the dielectrophoretic separator is presented in the preceding section. This section explains the theoretical analysis of the proposed physical structure.

Operation of the dielectrophoretic separator is based on the electric field gradient generated in the radial direction when a potential difference is applied between two concentric electrodes. Radius of the inner electrode, a, and the inner radius of the outer electrode affects the magnitude of the electric field indirectly. Considering the equation (3.1), only the ratio of these parameters affects the electric field magnitude. On top of that the effect is weakened due to the natural logarithm operation.



Inner electrode radius, a Outer electrode radius, b Initial spiral radius, r₀ Radius increment per turn, r_q

Figure 3.11: Design parameters of the spiral dielectrophoretic separator.

Expression of the electric field generated between coaxial lines which have infinite length is [17]:

$$\overrightarrow{\mathrm{E}(\mathrm{r})} = \frac{\mathrm{V}}{\ln(\mathrm{b/a})\,\mathrm{r}}\,\mathbf{a}_{\mathrm{r}} \tag{3.1}$$

where V is the magnitude of the potential difference applied, r is the distance from the center of the concentric electrodes, and $\mathbf{a_r}$ is the unit vector in the radial direction. It is evident that this expression is valid only for a < r < b condition. Another concern is that concentric electrodes, of course, do not have "infinite length". However, the formula is still correct for finite length electrodes provided that electric field lines which are confined into the length of the electrodes are calculated. Therefore, there is no inconvenience in using this formula for the z-axis points where thickness of the electrodes is greater. Up to now, an electric field, which depends on the radial distance travelled, is generated in the radial direction.

As indicated in the previous section, spiral microchannel is confined into the region between the electrodes. Spiral path originates from initial spiral radius, r_0 , and has a radius increment, r_q , per turn. Thus the radius of the path can be written as a function of angle θ as given below:

$$\mathbf{r} = \mathbf{r}_0 + \frac{\mathbf{r}_q}{2\pi} \mathbf{\theta} \tag{3.2}$$

It should be noted that θ is not necessarily to be bounded by 2π , in fact, it is certainly larger than 2π after a full cycle is completed. " θ " can be considered as the distance travelled in the angular direction in terms of radians.

Note that radial distance, r, becomes a function of θ with this equation, and therefore, the electric field generated becomes a function of θ , given by equation (3.3).

$$\overrightarrow{E(\theta)} = \frac{V}{ln(b/a)\left[r_0 + \frac{r_q}{2\pi}\theta\right]} \mathbf{a_r}$$
(3.3)

Finally, the electric field gradient between concentric electrodes is expressed as shown in the equation (3.4):

$$\overline{\nabla |\mathbf{E}(\theta)|^2} = \frac{\partial \overline{\mathbf{E}(\theta)^2}}{r \, \partial \theta} = -\frac{|\nabla^2|}{[ln(b/a)]^2 \left[r_0 + \frac{r_q}{2\pi}\theta\right]^4} \frac{r_q}{\pi} \mathbf{a}_{\theta}$$
(3.4)

This gradient is a result of a physical transformation which transforms electric field gradient in the radial direction to angular direction due to spiral geometry. Since $\overline{\nabla |E(\theta)|^2}$ is directed in the theta direction, dielectrophoretic force is also directed in the same sense; however direction can be either clockwise or counter-clockwise depending on the sign of the Clausius-Mossotti factor. It should also be noted that force is affected from the geometry parameters in the same sense $\overline{\nabla |E(\theta)|^2}$ is affected.

3.4 Design Parameters and Trade-Off

This section presents the limitations on design parameters and how they affect the performance criteria such as resolution, separation time, and accuracy. Moreover, trade-offs between these parameters is explained in detail.

Design parameters of the dielectrophoretic particle separator are

- radius of the inner electrode, a,
- inner radius of the outer electrode, b,
- ratio of radii of electrodes, b/a,
- initial spiral radius, r₀,
- radius increment per turn, r_q,
- channel width, w,
- number of spiral turns, N,
- electrode thickness, t, and
- channel height, h.

Radius of the inner electrode (a): This parameter affects the electric field gradient, and hence, the dielectrophoretic force. To maximize the force, inner electrode radius should be kept as close as possible to inner radius of the outer electrode radius, theoretically. In the limiting case, when a=b, the force between electrodes becomes infinity; however, there exists no space where force can be defined which is consistent with energy conservation. Still keeping "a" close to "b" maximizes the force; however, separation zone is reduced. Thus, to increase separation zone increasing both "a" and "b" in the same scale seems as a solution, but it has a major drawback. Note that radial distance in electric field equation, r, is measured from the center of the concentric electrodes. Thus, if radii of both electrodes are increased, starting value of "r", in fact "r₀" increases intrinsically. This drops down the force very fast, since force is inversely proportional with r_0^4 . As a result, "a" should be kept as close as possible to "b" and should be kept as small as possible by considering the area of separation zone.

Inner radius of the outer electrode (b): Mentioned limitations for inner electrode radius are also valid for this parameter. On top of that, "b" defines the layout area of a single dielectrophoretic particle separator.

Ratio of radii of electrodes (b/a): As equation (3.4) indicates as "b/a" ratio increases, the force decreases. Thus, as stated previously, this value should be kept as small as possible.

Initial spiral radius (r_0): This parameter defines the distance from the center of electrodes to the first point of the wall of the spiral microchannel. As stated in equation (3.4), r_0 should be minimized to maximize the dielectrophoretic force. Thus, r_0 should be kept as close as possible to "a"; however, this cannot be applied due to practical injection issues. Thus, the distance between "a" and " r_0 " should be kept as small as the practical issues allow. This parameter, also, affects the number of turns with radius increment per turn, " r_q ", since spiral microchannel is confined between " r_0 " and "b", practically.

Radius increment per turn (r_q) : The dielectrophoretic force is inversely proportional to r_q^3 , thus " r_q " should be kept as small as possible. However, as " r_q " decreases,

number of spiral turns, "N", increases which also increases the separation time and distance. Therefore, there is a trade-off between magnitude of force and separation time for this parameter. Another effect of " r_q " is observed in resolution performance. Since resolution is defined as $\Delta\theta$ for different particles, considering the equation (3.2) to reach the same Δr value with high $\Delta\theta$, r_q should be kept small. Also, for an intuitive approach, if r_q is kept small, then number of spiral turns between electrodes increases, thus, particles are exposed to DEP force for a longer time. Since the difference between particles is small, integration of this small difference over a longer time provides visible separation.

Channel width (w): This parameter is, in fact, another expression of " r_q " with only one difference: the thickness of wall between adjacent spiral turns. Note that w is intrinsically smaller than r_q . However, since it directly affects the value of " r_q ", it is considered as a design parameter. If "w" is kept small, keeping " r_q " small will be much easier. It can be anticipated that there is a lower limit for "w" which is due to the particle sizes. Channel width should allow at least a couple of particles to pass through. On the other hand, "w" should be kept as wide as possible to increase the effective potential difference across the channel. Considering series-capacitance modeling of the medium in the channel and channel walls, if channel width is kept wide, capacitance of the medium decreases, and hence, potential difference increases across the channel which means effective division of applied voltage.

Number of spiral turns (N): This parameter is not an independent parameter, it depends on " r_0 ", " r_q ", and "b". N is almost equal to $(b - r_0)/r_q$, thus selection of the mentioned parameters defines the number of spiral turns unless spiral is finalized before reaching the outer electrode. In this case, separation distance is directly proportional with "N".

Electrode thickness (t): Electrode thickness defines the maximum height at the channel where electric field distribution in z-axis is uniform. The necessity of uniform electric field distribution in z-axis is explained in the following section. The best case for electrode thickness is the height of the channel; however, due to fabrication limitations in lithography and electroplating, electrode thickness is kept smaller than channel height in practice.

Channel height (h): This parameter limits the size of the particles which are allowed to pass through as "w". It is preferred to have w=h for most cases due to square cross-section of the channel and symmetric distribution. Previously, it has been stated that "h" is intrinsically greater than "t"; however it should be considered that if h>>t, electric field distribution in z-axis will be non-uniform for most of the channel cross-section area.

In order to observe the results for various combinations of the given design parameters, design, simulation, and experimentation phases have been performed for 3 sets of devices.

In the following tables ranging from Table 3.1 to Table 3.3, mechanical dimensions used in the design are summarized with respect to device group. Note that in these tables parameters are given in micrometers.

Group	Name	а	b	r_0	r_q	w	t
1	DSC1.1	100	550	300	20	10	10
	DSC1.2					18	2
	DSC1.3				40	20	20
	DSC1.4		900	400	40	20	20
	DSC1.5					35	5

Table 3.1: Dimensions of DSC group 1 devices. All dimensions are in micrometers.
Group	Name	а	b	r_0	r_q	w	t
2	DSC2.1	100	1150	400	50	25	25
	DSC2.2					45	5
	DSC2.3		1200		80	40	40
	DSC2.4					75	5
	DSC2.5		1700		160	80	80
	DSC2.6					150	10

Table 3.2: Dimensions of DSC group 2 devices. All dimensions are in micrometers.

Table 3.3: Dimensions of DSC group 3 devices. All dimensions are in micrometers.

Group	Name	а	b	r_0	r_q	w	t
3	DSC3.1	200	1100	600	40	20	20
	DSC3.2	200	1100	600	40	30	10

This section has presented the design parameters and their dependencies on each other. The next section describes the advantages proposed with this design.

3.5 Advantages of the Design

As stated in the previous sections, this design has three major advantages:

- Concentric electrode configuration
- Spiral microchannel structure
- 3D electrode structure

First of all, the spiral channel geometry with coaxial electrodes enables much longer separation region with only two electrodes. This is important since as the exposure time for DEP forces becomes continuous, the effect of any instantaneous force is minimized, and hence the undesired variations at the output diminish. Also, spiral channel enables enough time and path for separating particles with close dielectric parameters or sizes which is equivalent to high resolution. Besides, as the particles are always in touch with outer walls, affinity separations can also be realized. For example, an antibody can be coated to the walls of the micro channels and cells having an affinity to this antibody can be captured, while others continue travelling.

3D electrodes are utilized to provide uniform electric field distribution in the z-axis. Since different size particles are under concern, it is critical to have uniformity in electric field distribution in the z-axis. The separation is supposed to be performed via non-uniform electric field generated in the x-y plane. Electric field line distributions for both 2D and 3D electrodes cases are illustrated in Figure 3.12:



Figure 3.12: Electric field line distributions for 2D and 3D electrodes where red particles denote the small particles and green ones denote the larger particles.

Figure 3.12 clearly indicates that

- electric field lines (fringe fields) get less concentrated above the electrodes in co-planar electrode configuration. Thus DEP force is decreased.
- 3D electrode configuration provides uniform force distribution on both particles.
- if co-planar electrodes are used, mostly fringe fields will be confined into channels whereas main electric field lines are confined into channels when 3D electrodes are used.

It should also be noted that if co-planar electrodes have been used, dielectrophoretic force in the z-axis will affect particles which have different sizes at different levels in magnitude sense, and the dielectrophoretic force created will be less with respect to 3D electrode configuration in the upper portion of the microchannel volume.

3.6 Simulations Based on FEM

Up to this section, analytical explanation of the dielectrophoretic particle separator is presented. This section presents numerical analysis of the physical structure in terms of electric field and dielectrophoretic force with the help of a finite element method simulation tool.

In order to observe the effects of each design parameter, three sets of design have been simulated via Generalized Electrostatics module of COMSOL 3.4 Multiphysics by utilization of Lagrange-Quadratic shape functions. Using the dimensions given in Table 3.1, Table 3.2, and Table 3.3, electric field and gradient of the square of the electric field of each dielectrophoretic separator are simulated. Simulation results of a single type are given in this section and the rest is given in the Appendix A.

First of all, all the geometries drawn in Cadence have been imported into COMSOL 3.4 Multiphysics, and then, subdomains are defined. Note that channel walls are made of parylene-C, and hence, it is defined as dielectric with relative permittivity of 3.10. Buffer solution is defined with relative permittivity of 78.5 and conductivity of

1.55 S/m [40]. Next, boundary conditions are set at the electrode boundaries for voltage application. Finally, the structures have been meshed and solver is run.

First, electric field analysis has been completed with a voltage of 1000 V DC, and then $\nabla |\mathbf{E}|^2$ is calculated by writing the following equation in the appropriate script [41]:

$$\nabla |\mathbf{E}|^2 = \mathbf{a}_{\mathbf{x}} \frac{\partial}{\partial \mathbf{x}} \left(\mathbf{E}_{\mathbf{x}}^2 + \mathbf{E}_{\mathbf{y}}^2 \right) + \mathbf{a}_{\mathbf{y}} \frac{\partial}{\partial \mathbf{y}} \left(\mathbf{E}_{\mathbf{x}}^2 + \mathbf{E}_{\mathbf{y}}^2 \right)$$
(3.5)

Electric field analysis is conducted in 2D since there will be a uniform distribution in the z direction due to 3D electrode geometry. Since other parameters in the force equation are constant for a defined test environment, checking the pattern and amplitude of $\nabla |\mathbf{E}|^2$ is usually sufficient to understand the behavior of the force.

For the device having an inner electrode radius of 100 μ m, an outer electrode radius of 1700 μ m, a spiral start radius of 400 μ m, a radius increment per turn of 160 μ m, and a channel width of 80 μ m, results for $|\mathbf{E}|$ and $\nabla |\mathbf{E}|^2$ are represented in Figure 3.13 and Figure 3.14, respectively. The simulations suggest that, average electric field and $\nabla |\mathbf{E}|^2$ values *inside* the channels are 2.2x10⁴ V/m and 9.6x10¹¹ V/m², respectively.

It is worthy to note that simulations related with the first three designs have also been performed. The simulation of the first design shows the dielectrophoretic traps which causes the particles stop at those points, the second design gives the least electric field magnitude inside the channels. The simulation of the third one resembles the final design only for the electrode height. Again, the amplitude of the electric field is less than the final design as the cross-section height gets closer to the height of the ceiling of the parylene channel.



Figure 3.13: COMSOL 3.4 Multiphysics simulation results for the device possessing the parameters a=100 μ m, b=1700 μ m, r₀=400 μ m, r_q=160 μ m and a channel width of 80 μ m. In this case, simulation results are limited between 2.05x10⁴ V/m and 2.4x10⁴ V/m to provide better representation of field distribution inside the channels.

Given these parameters and conditions, 10 μ m and 1 μ m beads are, theoretically, expected to move with average speeds of 534.2 μ m/s and 5.3 μ m/s, respectively. These values are calculated in accordance with equation (2.12). Simulation results prove that 1 μ m and 10 μ m beads can be separated in the proposed structure.

Also, it should be noted that the results deviate too much when irrelevant parts are included in the analysis. Simulation results and calculations of the average speeds of $1 \mu m$ and $10 \mu m$ particles for other types of devices are presented in the Appendix A.



Figure 3.14: COMSOL 3.4 Multiphysics simulation results for the device possessing the parameters a=100 μ m, b=1700 μ m, r₀=400 μ m, r_q=160 μ m and a channel width of 80 μ m. Simulation results are limited between 1.00x10¹¹ V²/m³ and 3.00x10¹² V²/m³ to provide better representation of $\nabla |\mathbf{E}|^2$ distribution inside the channels.

CHAPTER 4

FABRICATION AND EXPERIMENTATION OF THE DIELECTROPHORETIC SEPARATOR

This chapter, firstly, presents the fabrication of the spiral channel dielectrophoretic separator with concentric 3D electrodes. Then the experimental setup and method are introduced. Finally, the test results are compared with simulation results and the discussion on the results are given.

While planning of the fabrication flow of a dielectrophoretic separator, biocompatibility of the materials and the parameters of the design such as electrode height, channel width should be considered. Also, electrical and fluidic connections are also considered during layout creation phase. In this study, fabrication of the micro channels is performed via suspended parylene channel process which was developed by Prof. Mastrangelo [42]. Another aspect of fabrication is the gold electroplating step to increase the height of the electrodes to create a uniform electric field in the z-direction in the channel as explained in the design chapter. The channel material, Parylene-C, and the electrode material, gold, are known to be biocompatible. Moreover, glass wafer is selected as the base material to preserve the biocompatibility.

After fabrication of the devices with the aforementioned method, the dielectrophoretic separator has been tested and characterized in terms of output variation, separation resolution, and accuracy. The tests have been performed using polystyrene beads at different sizes to prove the size based separation of same type particles under the influence of dielectrophoretic forces.

As a final remark, the test results have been compared with the simulations results, and it has been shown that there is a good matching between them. Also, the reasons for the discrepancies have been discussed.

4.1 Fabrication Flow of the Structures

As mentioned previously, four different designs have been implemented. Fabrication flows of first three designs are explained briefly for the sake of simplicity, and fabrication flow of the final design is presented in detail.

4.1.1 Fabrication Flow of Design I

The first design is fabricated using 4-inch glass wafers. After BHF treatment of wafers, Cr/Au metallization and related photolithography step is performed to form the inner electrodes. After patterning the inner electrodes, a very thin Parylene-C layer is deposited on top the first metal in order to insulate inner and outer electrodes from each other. Next, second metallization and corresponding photolithography step is performed to create the Cr/Au outer electrodes. These two metallizations are performed using magnetron sputtering system. Then, channel forming lithography using thick photoresist is performed to pattern the channel volume. The channel material has been chosen as Parylene-C due to aforementioned properties. By deposition of parylene, the micro channels have been formed. Next steps aim to open up reservoirs and metal pad contacts. Therefore, a photolithography step with very thick photoresist has been performed to define the regions where reservoirs and contact pads are located. To etch the parylene-C at these regions, reactive ion etching has been performed. Finally, the channels are released using acetone, isopropanol, and methanol rinse cycle. Figure 4.1 illustrates the entire fabrication flow.



Release of channels

Figure 4.1: Fabrication flow of design I.

4.1.2 Fabrication Flow of Design II

The second fabrication flow is initialized with Cr/Au metallization of both sides of a 4-inch glass wafer. The metallization on the back side of the wafer is patterned to etch the glass wafer to create the surface for inner concentric electrode; however, the metallization on the front side has not been patterned at this step to prevent etching of glass from the front side. After etching of glass from backside with HF, the metallization at the back side has been stripped off. Since it has floating regions due to the undercuts formed during HF etching, this strip step has been performed. During removal of back side Cr/Au, the metallization on the front side has been protected by photoresist coating prior to metal etch. Next, metallization on the front side has been patterned to create the outer concentric electrodes. After that, metallization of back side of the wafer has been performed via sputtering, and hence inner concentric electrodes have been performed. The next steps constitute the formation of parylene suspended channels. After definition of channel volume with thick photoresist, parylene-C is deposited using chemical vapor deposition method. Then, definition of regions where fluidic openings and electrical contacts are located is performed by photolithography step which utilizes very thick photoresist. Reactive ion etching of parylene opens the mentioned contact and opening regions. Finally, the channels are released using acetone, isopropanol, and methanol rinse cycle. Figure 4.2 illustrates the entire fabrication flow of design II.



Cr/Au metallization of both sides of 4 inch glass wafer

Figure 4.2: Fabrication flow of design II.



Figure 4.2: Fabrication flow of design II (continued).

4.1.3 Fabrication Flow of Design III

The third fabrication is also performed using 4-inch glass wafers and utilizing 3 masks. The first step is the Cr/Au metallization of glass wafers after BHF treatment. Photolithography to pattern the concentric electrodes has been performed and Cr/Au has been etched accordingly. Therefore, electrode formation is completed with this first step. Next step is to define the channel volume using a thick photoresist. After forming the channel volume with thick photoresist, parylene-C deposition is performed to create the channel structure. Then, opening lithography to pattern the reservoirs and contact pads has been performed. Finally, reactive ion etching of parylene has been completed to open the fluidic openings and electrical contacts. To prepare the devices for testing, release of channels are performed with acetone, ispropanol, and methanol rinse cycle. Figure 4.3 illustrates the entire fabrication flow for design III.



Release of channels

Figure 4.3: Fabrication flow of design III.

4.1.4 Fabrication Flow of Design IV

4-inch glass wafers are cleaned in piranha solution (H₂SO₄:H₂O₂, 1:1) prior to processing to remove organic residues. In this fabrication flow, glass wafer is preferred due to its transparency and electrical insulation. Then, buffered hydrofluoric acid (BHF) (NH₄F:HF, 7:1) has been applied to the glass wafers for 1 minute to roughen the surface, and hence, to improve the adhesion quality of deposited metals. Note that roughness created on the glass wafer is just in the order of a few nanometers. Gold has been chosen as the electrode material since it is a noble metal which possesses a resistance to oxidation and corrosion. It should be anticipated that, during tests, buffer solutions containing water and ions will be in touch with the electrode. However, direct deposition of gold onto glass does not provide the required adhesion, especially after etching. Thus, it is decided to employ chromium as the adhesion layer. Therefore, chromium (Cr) and gold (Au) layers with 25 nm and 200 nm thicknesses have been deposited by sputtering (BESTEC Magnetron Sputtering), respectively.

Thicknesses are optimized such that chromium is deposited at the lowest thickness at which sputter can preserve uniformity and gold is deposited at the thickness which creates acceptable resistance values during gold electroplating to create 3D electrodes. Before performing gold electroplating, gold seed layer is patterned to eliminate the necessity of gold etching after gold electroplating which requires a new mask. To define the pattern which will be protected during gold etch, lithography is performed with AZ[®] 5214E Image Reversal Photoresist (MicroChemicals GmbH) [43]. AZ[®] 5214E is a very special photoresist which is capable of image reversal. Exposed areas may be selectively cross-linked by applying a bake cycle after exposure. A flood exposure before development converts unexposed areas soluble, resulting in a negative tone image which provides the patterning of gold seed layer with the same mask used for electroplating molding. After development of photoresist, gold has been shaped using commercial gold etchant (Transene) in 120 seconds to pattern the seed layer required to form electroplated concentric electrodes.

Next step is the preparation of the wafer for gold electroplating. First of all, patterned photoresist is stripped off using PRS-2000 Stripper (Baker) at 70°C for 20 minutes. Then, $AZ^{\text{(B)}}$ 9260 lithography has been performed to generate the electroplating mold. Photoresist height is measured as 9 µm. Since expected height of the electroplating is about 7 µm, the measured thickness is sufficient to perform uniform electroplating, otherwise electroplated gold will take the shape of a mushroom. Gold electroplating process has been performed using gold cyanide solution at 32°C (FIBRoplate process) to create 3D electrodes. After stripping the photoresist, heights of the electrodes are measured using Veeco Optical Surface Profiler and the thicknesses are found to be 7±0.5 µm.

Next, chromium adhesion layer between gold and glass has been etched in 60 seconds by using commercial chromium etchant (Transene) which is followed by dipping the wafer into 2% H₂SO₄ solution for 30 seconds to remove the Cr etchant residues from the surface of the wafer.

Up to now, 3D concentric electrodes are fabricated. Next step is to create the spiral micro channels. To fabricate microchannels, suspended parylene channel process is used. Parylene microchannel fabrication technology by releasing sacrificial photoresist has been developed by Prof. Carlos H. Mastrangelo [42]. In this process flow, firstly the volume of the channel is defined, secondly wall of the channel is created by parylene deposition, thirdly openings are created on parylene, and finally photoresist which defines the channel is stripped to release the channel. In this study, channel volume has been created with 16 μ m thick AZ[®] 9260 photoresist.

Channel walls have been formed by 20 μ m thick Parylene-C deposition using SCS 2010 Parylene Deposition System with 40 g Parylene-C dimer (SCS) onto AZ[®] 9260 photoresist layer. Before parylene deposition, a dicing tape is stick to the bottom of the wafer to prevent deposition of parylene on bottom surface since the deposition process is based on chemical vapor deposition. After that, the reservoir and electrode openings have been defined with AZ[®] 9260 lithography. Reservoir and electrode openings on parylene channels have been realized by Reactive Ion Etching (RIE, STS) in 90 minutes. Etching is performed in three cycles in order to reduce the thermal effects occurring due to the low temperature conductivity of glass.

After dicing, the sacrificial photoresist defining microfluidic channels are released by sequentially exposing devices to acetone (J.T. Baker), isopropanol (J.T. Baker), and methanol (J.T. Baker) for 6 hours, 30 minutes, and 10 minutes, respectively. Next, dies are dried on 70°C hotplate during 2 minutes. Fabrication flow of design IV is illustrated in Figure 4.4, and Figure 4.5 shows the fabricated DEP devices.

As an alternative fabrication flow, PDMS can be utilized instead of Parylene-C to form the structural material for the channel layer. It is obvious that this alteration will reduce the cost and remove the necessity for high-class clean room environment during the microfabrication. However, since the ultimate goal for this study is to integrate DEP separator onto a lab-on-a-chip, Parylene-C is preferable since further fabrication steps (e.g. deposition) can be performed.



Lithography and etching of Au to pattern electroplating area



Electroplating mold lithography and Au electroplating



Cr etch, channel forming lithography and parylene-C deposition



Opening lithography and parylene RIE



Release of channels

Figure 4.4: Fabrication flow of design IV.



Figure 4.5: Fabricated dielectrophoretic separators. (a) Wafer level devices with dicing, (b) a single device containing three identical spirals, (c) optical microscope image of a single spiral device.

4.2 Experimental Setup

The experimental setup was constructed for performing dielectrophoresis with high voltages and fluorescence based detection of the separation process. Online monitoring of the dielectrophoresis application was performed using Olympus SZX12 stereo microscope with fluorescence attachment. The attachment has a 100 W mercury lamp for illumination. For monitoring of the process, a high resolution digital camera, Olympus DP70, which was directly connected to a computer, was used. For the illumination and monitoring, a filter set with 460 nm band-pass excitation filter, 495 nm long-pass emission filter, and 485 nm long-pass dichromatic mirror was placed into the microscope. A high voltage DC supply is used for voltage application. The test setup is illustrated in Figure 4.6 and the final experimentation setup is given in Figure 4.7.



Figure 4.6: Illustration of test setup prepared to perform high voltage DC dielectrophoresis and monitoring of the moving particles using a CCD camera mounted microscope with fluorescent attachment.

The devices are placed on a custom designed package for electrical interfacing. Also a micromanipulator to contact the probe tip to inner electrode is prepared and wired. Voltage supply is connected to device inputs via the package electrodes and probe tip. In order to prevent the excessive drying due to high electrical voltage and optical illumination, humidity of the environment is kept constant at a sufficient level. This is achieved by placing the chip holder into a petri-dish which has a DI water reservoir and an opening to allow the electrical connections. The vapor pressure of the DI-water keeps the humidity of the environment in the required levels. Note that the external equipment needed for device operation can be found in any biomedical laboratory.



Figure 4.7: Test setup used for performing high voltage DC dielectrophoresis tests using a fluorescent microscope with a CCD camera for online monitoring.

4.3 Experimental Method (DC Dielectrophoresis)

The experimental procedure is as follows: Phosphate Buffered Saline (PBS) is first loaded into channels by placing a droplet on central opening of the devices. Then, the capillary action is enough to fill the microfluidic channels in a few seconds. After that, a DC voltage of 1000 V is applied to stabilize the electrokinetic effects on the flow. The expected electric field amplitude inside the channels is around $2.2x10^4$ V/m for the DSC2.5 type device (Table 2.2). It has been previously shown that this value of electric field is enough for dielectrophoretic forces to overcome electroosmotic flows induced by DC voltage application [21]. For testing purposes Fluoresbrite® YG Microspheres 10.0 µm, Polysciences Inc. and Polybead® Polystyrene Red Dyed Microsphere 1.00 µm, Polysciences Inc. are loaded into the center reservoir using a Hamilton microliter syringe.

To observe the movement of particles, fluorescence shutter is opened and the video recorder is turned on. Video is recorded with 25 frames per second (FPS) and processed using Particle Tracker plugin of ImageJ, an open source software [44]. Speed values for each experiment are calculated by processing approximately 125 frames which correspond to 5 seconds. It can be inferred that time required for 1 μ m polystyrene beads reaching the end point is around 2500 seconds, which corresponds to approximately 40 minutes. A typical snapshot of the recorded video is shown in Figure 4.8.



Figure 4.8: A typical snapshot of the recorded video.

4.4 Test Results and Discussions

Expected Results: In this experimental study, by using DC electric fields, size based separation is aimed. This is due to the fact that in the lower frequency limit approaching to DC, Re(f_{CM}) approaches -0.5 for polystyrene particles [45]. Hence, by equation (2.12) we can estimate that the speed for experiment parameters given in section 3.6 (or the travelled distance per given time) should be proportional to R². For 1 µm and 10 µm diameter particles used within the same device, the speed ratio should be 1:100 which is consistent with simulation results. Note that for 1 µm and 10 µm beads simulated speeds are found to be 5.3 µm/s and 534.2 µm/s, respectively.

Experimental Data: Figure 4.9 shows a comparative histogram of extracted speeds of 1 μ m and 10 μ m, where data bars show the number of bead counts for given speed interval and the straight lines show the best Gaussian fits for normalized amplitude.

Data indicates that 1 μ m particles have an average speed of 4.57 μ m/s with a standard deviation of 1.06 μ m/s, and 10 μ m particles have an average speed of 544 μ m/s with a standard deviation of 105 μ m/s. There is a -14% and +2% deviation from the simulation results for 1 μ m and 10 μ m beads, respectively. Moreover, DEP devices with planar electrodes have been tested; however, it is observed that electric field gradient is not sufficient to perform a separation.

Output Variation: Using the experimental data, the coefficient of variation for the speed for 1 μ m and 10 μ m beads can be calculated as 23% and 19%, respectively. On the other hand, microparticles have also some size variation due to production. The reported size variation by the supplier is 3% and 10%, which corresponds to a speed variation of 6% and 21% for 1 μ m and 10 μ m particles, respectively. While expected and recorded variations greatly overlap for 10 μ m size particles, there is a considerably big discrepancy between expected and recorded parameters in the case of 1 μ m size particles. This can be attributed to difference of Brownian Force acting on the particles. The Brownian motion greatly increases the speed-spread in 1 μ m case; however, for 10 μ m particles there is no significant effect of the Brownian Force. Hence, for the worst case of 1 μ m beads, it can be inferred that the output speed variation is 20%, corresponding to a size variation of 10%.

Quantization Resolution: To define the resolution, the worst case of output variation, that is, the 1 μ m bead experimental results, is taken into account. The device has shown around 20% coefficient of variation in speed, which can be assumed as a standard deviation of the speed introduced by device. It is defined that two successive peaks (Figure 4.9) are discriminable if they are approximately 2 standard deviations apart. This definition can be interpreted as two different size beads with radii R₁ and R₂ are discriminable under proposed experimental condition if R₁ \leq 0.81 R₂ or equivalently 1.21 R₁ \geq R₂.

Accuracy: While the actual size ratio of the input beads are 1:10, the device output suggests that the speed ratio is 1:119, corresponding to a 1:10.9 size ratio. Hence, the accuracy of size extraction from experimental data within 1 μ m to 10 μ m range can be calculated as $\pm 10\%$.

The devices other than DSC2.5 type device haven't provided consistent speed information; therefore, only comparison of test results and simulation results of DSC2.5 device is presented. Possible reasons for failure in the remaining devices are insufficient force due to less $\nabla |\mathbf{E}|^2$, adhesion of polymeric beads to the channel walls, capacitive sharing of applied voltage between channel walls and medium, and therefore inefficient voltage usage.

Consequently, here, a direct dielectrophoretic device with reduced operational cost and complexity and moderate separation accuracy and resolution is presented. This is primarily achieved by spiral channel architecture with coaxial electrodes keeping the device footprint minimum, while keeping the functional separation length maximum, and, hence, decreasing the costs. This architecture also proportionally decreases the other instantaneous effects while keeping enough channel length for distinguishing close parameter particles. Next, injection of the sample fluid to the channels by capillary action eliminates the need for external fluidic equipment and interconnections. The proposed device also capable of working with single power supply, which has also was become common laboratory equipment due to gelelectrophoresis kits. The experiments have shown moderate device performance with 10% accuracy and 20% of radius resolution with a simple stereo microscope.



Figure 4.9: Comparative histogram of extracted speeds of 1 μ m and 10 μ m beads, where data bars show the number of bead counts for given speed interval and the straight lines show the best Gaussian fits for normalized amplitude. Please note the break in the horizontal axis.

CHAPTER 5

CONCLUSIONS AND FUTURE RESEARCH OBJECTIVES

In this thesis, design, simulation, fabrication, and experimentation of a novel dielectrophoretic particle separation system have been performed. A direct dielectrophoresis based particle separation device capable of producing versatile chromatograms is developed. Device is novel with spiral channels and concentric electrodes, and requires only external voltage supplies for operation.

Separation techniques in the literature have been investigated, and methods are compared to each other in terms of practical applications. As a result, direct dielectrophoresis, which is an electrical separation method, has been chosen to be applied. Dielectrophoresis is a method which works with neutral particles under AC and DC voltages independent of voltage polarity. Thus, various separations become possible due to its versatile nature.

After examining the theory of dielectrophoresis deeply, requirements and expected results are defined for particle separation applications. Depending on these parameters, designs reported in the literature have been examined and advantages and disadvantages of these designs have been extracted. On this theoretical background a design has been initialized and verified using simulation tools utilizing finite element method. The first design, of course, has some disabilities; therefore, successive modifications have been performed on the first draft. Finally, a design

overcoming dielectrophoretic traps, fabrication related problems, testing problems has been proposed.

The final device is fabricated using parylene suspended channel process with 3D electrode geometries. Process developed for dielectrophoretic spiral chromatography requires just 3 masks. Various process steps are optimized and possible problems regarding fabrication are discussed. Fabricated devices are ready to use without additional post-processing such as surface coating or labeling protocols.

Dielectrophoretic particle separator requires a simple test setup consisting of a power supply and a microscope connected to a PC to record the experimentation on-line. Experimentation procedure has been introduced step-by-step in order to generate repeatable experiments in the future. During the experimentation satisfactory results have been achieved and discussions on separation performance based on resolution and accuracy have been presented. Moreover, simulation results have been compared with experimental results, and a great matching has been observed.

Up to now, what has been performed and achieved is introduced. Of course, it has related future works as all scientific studies. Future works concentrate on the optimization of the device design with respect to the difficulties during testing, optimization of experimentation, and conducting extensive tests for different cell samples to observe which biological agents are suitable for separation in this device.

Design should be modified to allow standard fluidic connections and to enhance the dielectrophoretic force. Note that basic method to enhance the force is to decrease the radius of the inner electrode, however, it directly causes resolution problems due to shorter separation distance, and therefore there is a trade-off that should be considered while enhancing the dielectrophoretic force. For the experimentation phase, buffer solutions employed should be optimized such that neither the dielectrophoretic force nor the living cells is affected negatively. As the ultimate goal, an electrical detection system should be integrated such that dielectrophoretic particle separation device will be a stand-alone portable device.

This chapter has explained the checkpoints reached in this thesis study and the targets to be reached have been set. Another aspect of this chapter is to explain the values added to the literature and possible practical applications of the proposed dielectrophoretic particle separator.

First of all, the design concept of spiral microchannels confined between concentric electrodes is introduced. With this design a method to convert radial electric field gradient into theta direction has been developed and regarding scientific articles have been published. On top of that using 3D electrodes in the design, non-uniformity in the xy-plane and uniformity in the z-axis have been achieved in terms of electric field. This development has added a new fabrication method into the inventory of METU BioMEMS Research Group.

As mentioned previously, proposed dielectrophoretic particle separator is aimed to be employed in clinical applications. Since all the materials that will be in touch with biological agents are biocompatible, there are various application areas for the fabricated devices. Here, some of them are introduced. First of all, separation of blood cells is used widely in the diagnosis of almost all illnesses. Moreover separation of sub-populations of a certain blood cell such as lymphocytes is crucial in differential diagnosis.

Another application area is to separate fertilizable and non-fertilizible eggs by means of the differences in cytoplasmic conductivities, and hence, the differences in Clausius-Mossotti factors. Finally, dielectrophoresis is utilized in separation of dead and alive cells from each other. This application is commonly useful in primary tests of new generated drugs on certain cell cultures which reveal the side effects of the drug on alive cells.

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APPENDIX A

FEM SIMULATIONS OF ALL SETS OF DEVICES

In this chapter, finite element method simulations of all devices are presented. The devices are named with their geometric properties. For instance, the device which has an inner electrode radius of 100 μ m, outer electrode radius of 1150 μ m, spiral channel initial radius of 300 μ m, radius increment per turn of 40 μ m, and channel width of 25 μ m is named as 100a_1150b_300r_40q_20w. All the devices are listed in Table 3.1 - Table 3.3. All the simulations are performed with 1 kV potential difference. In order to provide better understanding of the distribution of $\nabla |\mathbf{E}|^2$, the ranges are adjusted manually. Otherwise the graphs present a constant color due to very small values which are located on the electrodes and very high values which are located in discontinuities in the drawing. By adjusting the display range, these irrelevant parts are omitted in the figures, and they are shown as white.



Figure A.1: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_550b_300r_20q_10w.



Figure A.2: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_550b_300r_20q_18w.



Figure A.3: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_550b_300r_40q_20w.



Figure A.4: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_900b_400r_40q_20w.



Figure A.5: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_900b_400r_40q_35w.



Figure A.6: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_1150b_400r_50q_25w.


Figure A.7: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_1150b_400r_50q_45w.



Figure A.8: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_1200b_400r_80q_40w.



Figure A.9: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_1200b_400r_80q_75w.



Figure A.10: $\nabla |\mathbf{E}|^2$ distribution of the device 100a_1700b_400r_160q_150w.



Figure A.11: $\nabla |\mathbf{E}|^2$ distribution of the device 200a_1100b_600r_40q_20w.



Figure A.12: $\nabla |\mathbf{E}|^2$ distribution of the device 200a_1100b_600r_40q_30w.